

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE  
PATENT COOPERATION TREATY**

Authorized Officer Shane Thomas :  
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In Re Application of : METHOD AND APPARATUS FOR  
:  
RJ LEE GROUP, INC. : CLARIFICATION OF PYROLYSIS OILS  
:  
: Attorney Docket No. 287122-0159P  
International Application No. :  
PCT/US2018/052102 :  
:  
International Filing Date :  
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**ARTICLE 19 AMENDMENTS**

April 16, 2019

International Bureau of WIPO  
34 chemin des Colombettes  
1211 Geneva 20  
Switzerland

Sir:

Applicant submits herewith the attached AMENDMENTS TO THE CLAIMS (Claims 1-54) on pages 11-15 of the originally filed application.

Applicant also submits herewith a complete REPLACEMENT SET of the claims (Claims 1-52) as amended on pages 11-18, in substitution of all the claims originally filed in the above-identified International Application.

Applicant respectfully requests that the attached sheets of claims be entered in this application and that international preliminary examination include these replacement sheets.

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## AMENDMENTS TO THE CLAIMS

What is claimed is:

1. (Original) A method of processing pyrolysis oil comprising adjusting the polarity of said oil with a non-polar solvent,  
5 binding unwanted components to clay,  
eluting the clean oil in the non-polar solvent, and  
separating the non-polar solvent from the oil.
  
2. (Currently amended) The method of claim 1 including  
10 employing an alkane ~~of~~ as said non-polar solvent.
  
3. (Original) The method of claim 2 including  
employing an alkane selected from the group consisting of alkanes having 4 to 10  
15 carbons.
  
4. (Original) The method of claim 2 including  
employing a mixture of two or more alkanes selected from the group consisting of  
alkanes having 4 to 10 carbons.
  
- 20 5. (Original) The method of claim 2 including  
Employing an alkane selected from the group consisting of alkanes having 5 to 7  
carbons.
  
6. (Original) The method of claim 2 including  
25 employing hexane as said alkane.
  
7. (Original) The method of claim 2 including  
mixing said oil and alkane to adjust polarity.
  
- 30 8. (Original) The method of claim 7 including

mixing said oil and alkane preferably in a ratio of oil to alkane to about 1:2 to 1:30.

9. (Original) The method of claim 7 including

5 mixing said oil and alkane preferably in a ratio of oil to alkane to about 1:4 to 1:15.

10. (Original) The method of claim 7 including

10 mixing said oil and alkane most preferably in a ratio of oil to alkane to about 1:6 to 1:10.

11. (Original) The method of claim 7 including

after mixing said oil and alkane allow it to sit for at least 30 minutes to allow precipitation.

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12. (Original) The method of claim 1 including

effecting said separation of said solvent from said oil by evaporation.

13. (Original) The method of claim 1 including

20 employing attapulgit as said clay.

14. (Original) The method of claim 1 including

prior to a cycle of said process activating said clay.

25 15. (Original) The method of claim 1 including

said ratio of clay to oil being about 4:1 to 20:1 by weight.

16. (Original) The method of claim 1 including

said ratio of clay to oil being about 6:1 to 15:1 by weight.

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17. (Original) The method of claim 1 including  
cleaning said clay before performing a next cycle of said processing of said  
pyrolysis oil.
- 5 18. (Original) The method of claim 17 including  
employing a polar solvent to clean said clay.
19. (Original) The method of claim 18 including  
employing acetone as said clay cleaning polar solvent.
- 10 20. (Original) The method of claim 17 including  
employing as said clay cleaning polar solvent a material selected from the group  
consisting of methanol, tetrahydrofuran and dimethylformamide.
- 15 21. (Original) The method of claim 1 including  
employing a column in performing the processing of said binding unwanted  
components to clay.
22. (Original) The method of claim 21 including  
20 employing hexane as said alkane in said oil and alkane mixture.
23. (Original) The method of claim 22 including  
creating flow of said oil-alkane mixture through said column at the rate of about  
0.1 to 0.6 liters per hour of column flow per liter of column void volume.
- 25 24. (Original) The method of claim 21 including  
employing hexane as said alkane in said oil and alkane mixture, and

creating flow of said mixture through said column at the rate of about 0.2 to 0.4 liters per hour of column flow per liter of column void volume.

25. (Original) The method of claim 1 including,

5 employing hexane as said alkane in said oil and alkane mixture, and

creating flow of said mixture through said column at the rate of about 0.3 to 3.5 liters per hour of column flow per liter of column void volume.

26. (Original) The method of claim 1 including

10 effecting said separation of said non-polar solvent from said oil by heating said mixture to a temperature high enough to evaporate said non-polar solvent but not high enough to evaporate said oil.

27. (Original) The method of claim 1 including

15 effecting said separation of said non-polar solvent from said oil by heating said mixture to between the boiling point of the non-polar solvent and 32°C above the boiling point of the most volatile compound in the particular pyrolysis oil fraction.

28. (Original) The method of claim 1 including

20 effecting said separation of said non-polar solvent from said oil by heating said mixture preferably to between the boiling point of the particular solvent and 10°C above the boiling point of the most volatile compound in the particular pyrolysis oil fraction.

29. (Original) The method of claim 1 including

25 effecting said separation of said non-polar solvent from said oil by heating said mixture to between the boiling point of the particular solvent and 2°C above the boiling point of the most volatile compound in the oil fraction.

30. (Original) The method of claim 20 including  
employing hexane as said non-polar solvent and heating said mixture to between  
68°C to 100°C to evaporate said hexane.
- 5 31. (Original) The method of claim 20 including  
employing hexane as said non-polar solvent and heating said mixture to preferably  
between 68°C and 78°C to evaporate said hexane.
32. (Original) The method of claim 1 including  
10 effecting said processing by employing a distillation-elution method.
33. (Original) The method of claim 1 including  
effecting said processing by forced flow elution methods.
- 15 34. (Original) The method of claim 12 including  
condensing said evaporated alkane,  
introducing said condensed alkane into a first vessel,  
said oil being in a second vessel, and  
said second vessel being substantially alkane free.
- 20 35. (Original) The method of claim 14 including  
regenerating said clay with a polar solvent, and  
reactivating said regenerated clay.
- 25 36. (Canceled)
37. (Currently amended) Apparatus for processing pyrolysis oil comprising ~~The~~  
apparatus of claim 36 including

a first vessel for receiving a mixture of said pyrolysis oil and a non-polar solvent,

a heater for evaporating said non-polar solvent,

a first condenser for receiving said evaporated non-polar solvent and condensing the same, and

5 a clay column for receiving condensed vapors from said condenser and eluting said non-polar solvent therefrom into a second vessel.

38. (Currently amended) The apparatus of claim 37 ~~36~~ including  
said apparatus structured to deliver said evaporated non-polar solvent to a second  
10 vessel leaving said oil in said first vessel.

39. (Original) The apparatus of claim 38 including  
said first vessel structured to receive substantially all of said pyrolysis oil and to  
be substantially devoid of said non-polar solvent.

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40. (Currently amended) The apparatus of claim 37 ~~36~~ including  
said apparatus structured to clean said clay column after a cycle of operation.

41. (Original) The apparatus of claim 40 including  
20 said apparatus structured to employ acetone as said clay cleaning polar solvent.

42. (Currently amended) The apparatus of claim 37 ~~36~~ including  
said apparatus structured to process non-polar solvents which are alkanes having 4  
to 10 carbons.

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43. (Original) The apparatus of claim 41 including  
said apparatus structured to process hexane.

44. (Currently amended) The apparatus of claim ~~36~~ 37 including  
said apparatus structured to function as distillation apparatus in processing said  
pyrolysis oils.

5 45. (Currently amended) The apparatus of claim ~~36~~ 37 including  
said apparatus being employable in both the processing of said pyrolysis oils and  
the cleaning of said apparatus after a cycle of operation.

46. (Currently amended) An apparatus for processing pyrolysis oils comprising  
10 a first vessel for holding a mixture of said oil and a non-polar solvent,  
a clay column for receipt of said mixture,  
a second vessel for receiving said mixture passing through said clay column,  
said second vessel structured to heat said mixture to a temperature at which said  
non-polar-solvent will vaporize, but said oil will not vaporize.

15 a condenser for condensing said vapors, ~~and~~  
a third vessel for receipt of said condensed vapors until only oil remains in said  
second vessel, and  
delivery means for delivering a clay cleaning material to said clay column after a  
cycle of operation.

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47. (Original) The apparatus of claim 46 including  
said apparatus structured to process non-polar solvents which are alkanes having 4  
to 10 carbons.

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48. (Original) The apparatus of claim 46 including  
said apparatus structured to process a non-polar solvent which is hexane.

49. (Currently amended) The apparatus of claim 46 including  
30 said apparatus structured to simultaneously process a plurality of non-polar  
solvents which are alkanes having 4 to 10 carbon, ~~simultaneously.~~



50. (Canceled)

51. (Currently amended) The apparatus of claim ~~46~~ 50 including  
5 said clay cleaning material being acetone.

52. (Currently amended) The apparatus of claim ~~46~~ 50 including  
said clay being attapulgite.

10 53. (Original) The apparatus of claim 52 including  
said apparatus structured to activate said clay before performing a next cycle of  
said processing of pyrolysis oil.

54. (Currently amended) The apparatus of claim 53 including  
15 said apparatus structured to effect said activation by drying said clay ~~at~~ up to  
about 150°C until there is no more weight loss.